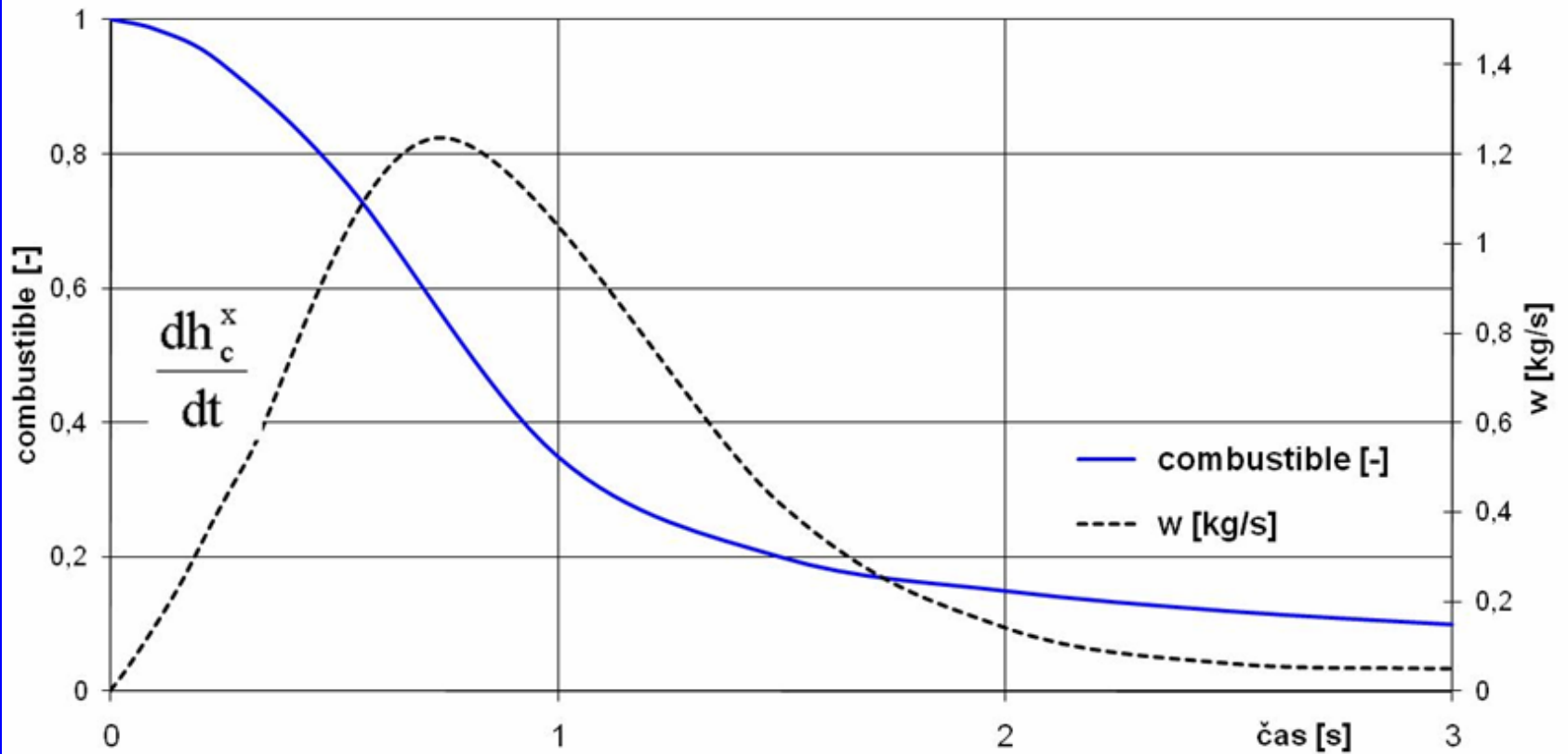


Coal characterization with use of drop tube test facility

Radim Paluska



Burnout velocity of pulverized coal with $d = 142 \mu\text{m}$, $t = 1000^\circ\text{C}$ and excess of air $n = 1,24$



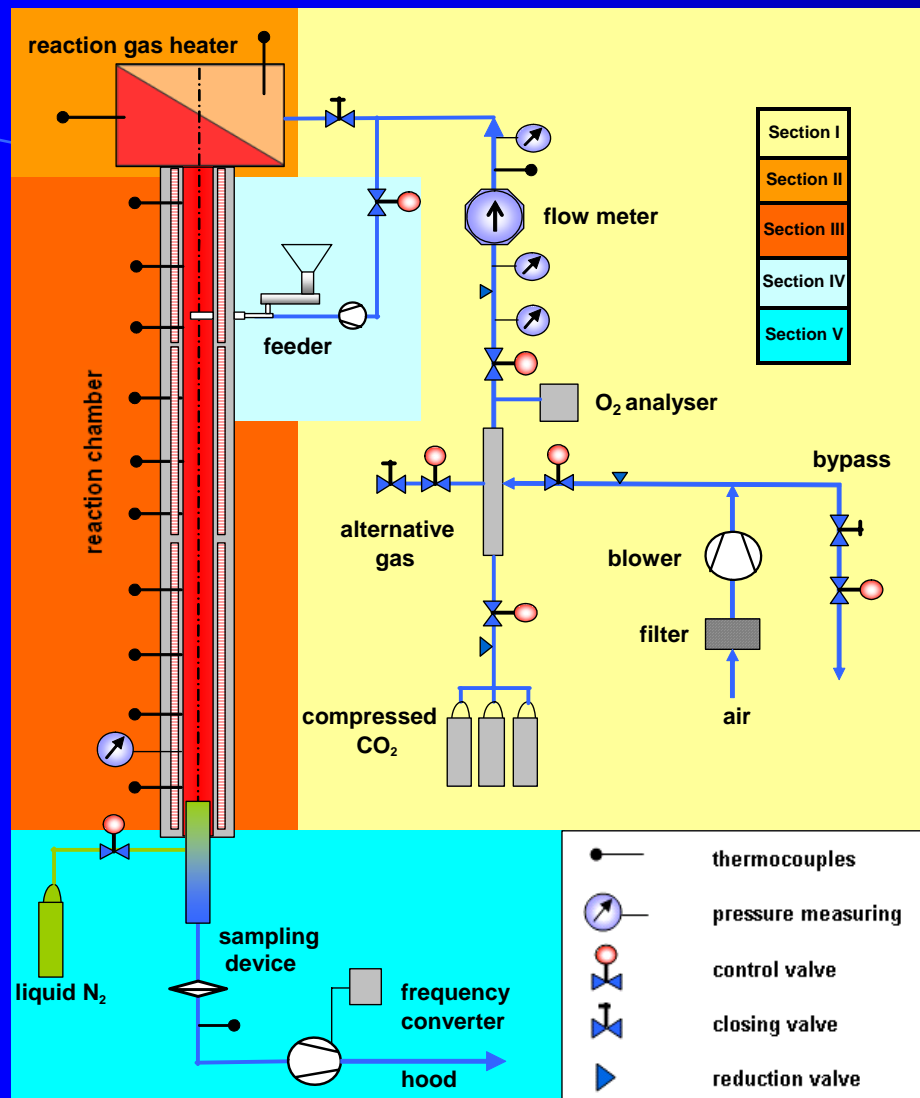
Thermokinetic properties of pulverized coal

Arrhenius equation

$$k = Ae^{-E_a / RT}$$



Drop tube



Parameters of ERC drop tube

- 5 m long reaction chamber, 66 mm inner diameter
- Temperature in reaction chamber up to 1200 °C
- Reaction gas velocity 1 – 4 m.s⁻¹
- Concentration of oxygen 0 – 21 %



- **4 degrees of freedom**

1. **Reaction gas temperature**
2. **Concentration of oxygen**
3. **Reaction gas velocity**
4. **Sample grain size**

- **Time-consuming and expensive tests and analyses**



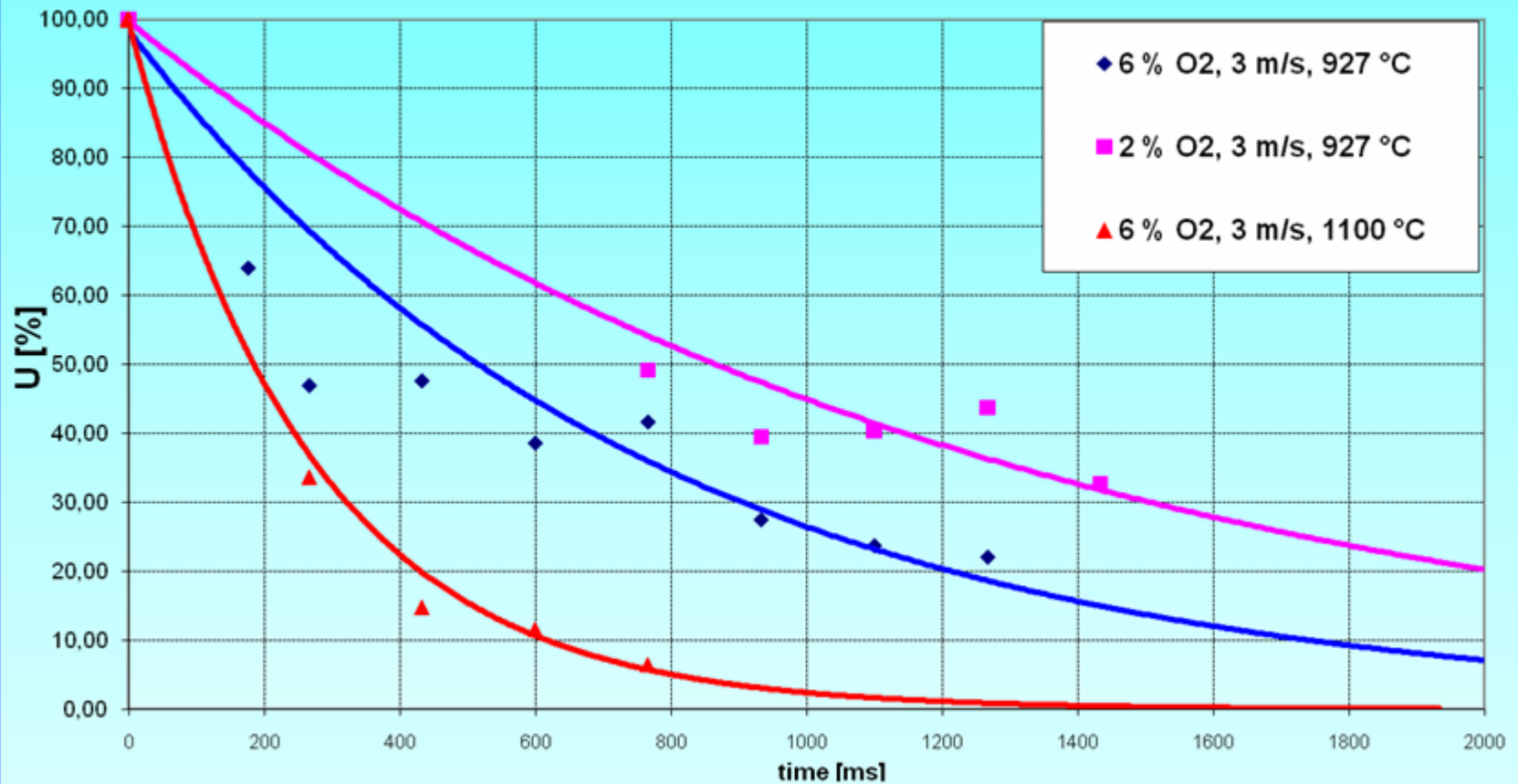
Input parameters of used sample

Proximate analysis		
Moisture	%	1.23 %
Ash	%	21.27 %
Volatiles	%	26.27 %
Fixed carbon	%	51.23 %
Other parameters		
Particles temperature	°C	20
Mass flow of particles	g.s ⁻¹	5,56E-03
Rosin-Rammler index	N 1,26 x 39,87 μm	

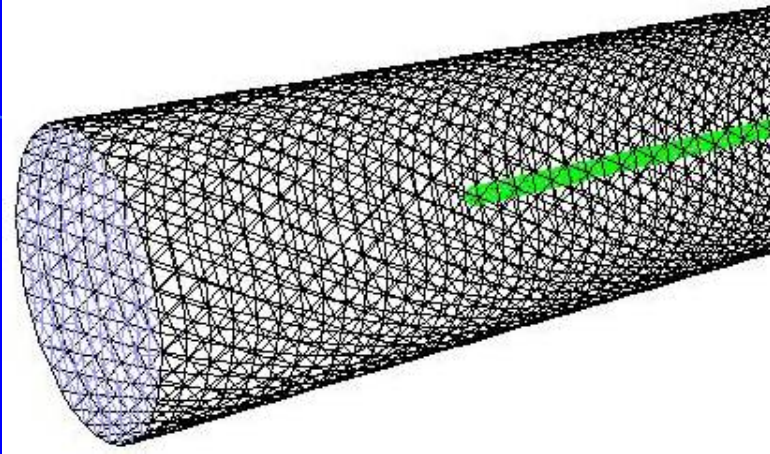


Results obtained from experiments

VZ 670/09 - black coal ETB, grain size 80-90 μm



Model in program Fluent



Devolatilization

$$T_p \geq T_{vap}$$

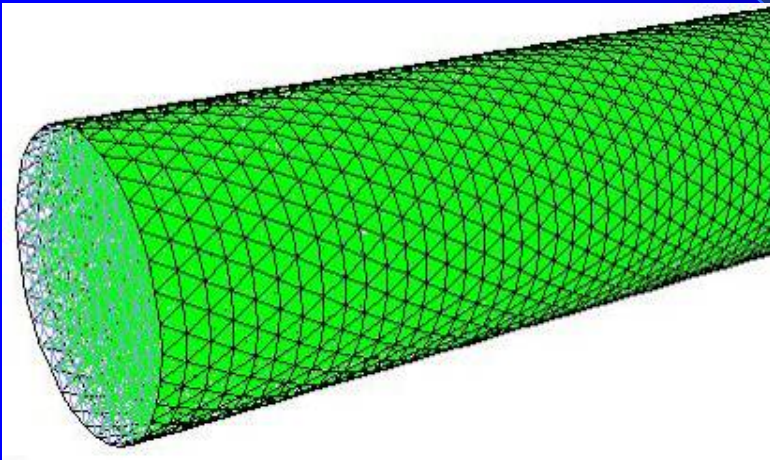
$$m_p \rangle (1 - f_{v,0})(1 - f_{w,0}) m_{p,0}$$

The single kinetic rate model

$$-\frac{dm_p}{dt} = k [m_p - (1 - f_{v,0})(1 - f_{w,0}) m_{p,0}]$$

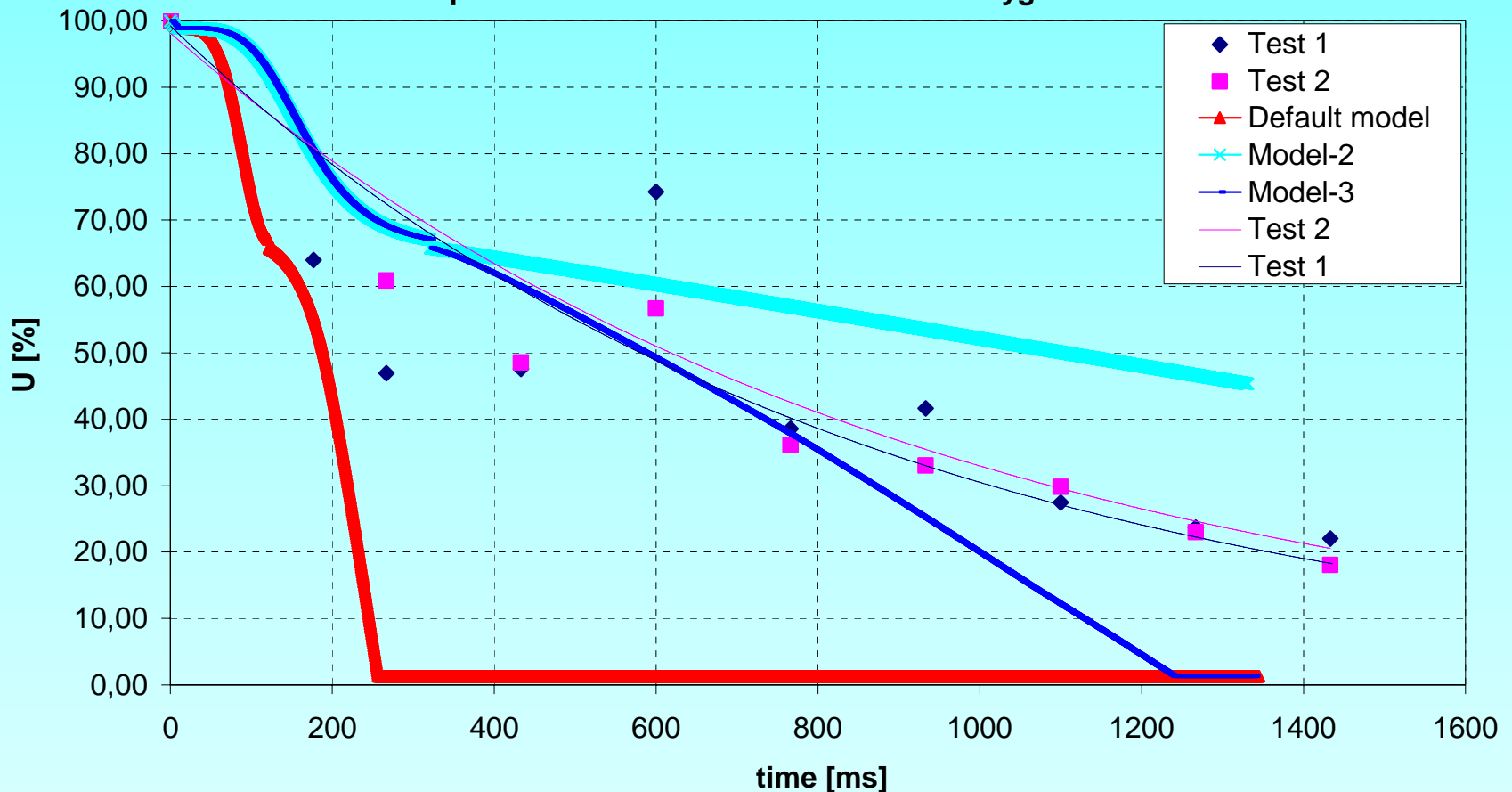
Char combustion

$$m_p \rangle (1 - f_{v,0} - f_{comb})(1 - f_{w,0}) m_{p,0}$$



Modelling of experimental results in Fluent

Burnout of pulverized black coal under reaction gas velocity 3 m/s,
temperature 927°C and concentration of oxygen 6 %



Kinetic constants obtained from model

	Default model	Model 2	Model 3	Model 4
A (1)	312 000	312 00	312 00	?
E1 (J Kmol)	7.4 e+07	7.4 e+07	7.4 e+07	?
C1 (1)	5,00E-12	5,00E-12	5,00E-12	?
C2 (1)	0.002	0.0002	0.00045	?
E2 (J Kmol)	7.9e+07	7.9e+07	7.9e+07	?



Thank You for attention

